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PATENT APPLICATION

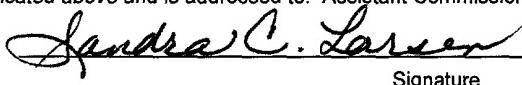
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PROCESS FOR RECOVERY OF OLEFINICALLY UNSATURATED
NITRILES

by

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BACKGROUND OF THE INVENTION

This application is a continuation-in-part of Application Serial No. 09/333,431, filed June 15, 1999, entitled "Process for Recovery of Olefinically Unsaturated Nitriles."

The present invention relates to a process for the recovery and purification of an olefinically unsaturated nitrile, such as acrylonitrile, from a reactor effluent stream.

Processes for the production of olefinically unsaturated nitriles by the catalytic reaction of ammonia and an olefin are well known. For example, acrylonitrile and methacrylonitrile may be produced by the vapor phase catalytic oxidation of propylene and isobutylene, respectively, in the presence of ammonia.

In commercial processes for preparation of acrylonitrile from propylene, ammonia, and oxygen, the reactor effluent contains, in addition to the desired acrylonitrile product, considerable amounts of by-product hydrogen cyanide, acetonitrile, and other impurities such as succinonitrile and other nitriles. The exact composition of the effluent and the by-products and impurities it contains may vary considerably depending on the ammonoxidation reaction conditions and catalyst. Reactor effluents from processes for producing other olefinically unsaturated nitriles similarly contain various byproducts or impurities.

Processes for treating reactor effluents of the type described to separate and recover acrylonitrile product from by-products or impurities are known. For example, see U.S. patents 3,399,120, 3,433,822, 3,936,360, 4,059,492, 4,166,008, and 4,404,064, which are incorporated herein by reference. Typically, these processes include introducing the reactor effluent into a quench chamber where it is contacted with water (usually containing sulfuric acid to neutralize excess ammonia from the reaction) to cool the effluent and remove some contaminants such as polymers produced in the reactor. Cooled effluent gases from the quench flow to an absorber column where they are contacted with water. The liquid stream from the bottom of the absorber column contains most of the nitriles produced in the reaction and some impurities, and is sent to an extractive distillation column, also referred to as the recovery column. The major portion of the acrylonitrile from the extractive distillation column is obtained in the overhead (distillate) from the recovery column while water and impurities constitute most of the

1 bottom stream from the recovery column. The bottom stream is typically fed to a
2 secondary distillation or stripper column to separate acetonitrile and water in an overhead
3 stream while the secondary column bottoms containing water and various impurities are
4 recycled, for example to the quench column.

5 U.S. Patent No. 3,399,120 describes an embodiment in which acrylonitrile is
6 purified utilizing a single recovery and stripper column. However, an enrichment column
7 is required to concentrate and separate the acetonitrile from the acrylonitrile and water
8 mixture.

9 The use of two or more columns, the recovery column, the stripper column and/or
10 the enrichment column, is effective to achieve the product separation and recovery that is
11 required in commercial operations. However, this system is expensive, due both to the
12 cost of the equipment involved (not only the two or more columns, but also the associated
13 pumps, piping, heat exchangers, etc.) and the operating costs such as energy usage by the
14 two columns. A need exists for improved processes that can achieve the desired recovery
15 at a lower cost.

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17 SUMMARY OF THE INVENTION

18 A process for the recovery of acrylonitrile from a stream comprising acrylonitrile,
19 water, and organic impurities, comprises the steps of (a) quenching an ammonoxidation
20 reactor effluent stream that comprises acrylonitrile, water, and organic impurities with an
21 aqueous quench stream, thereby producing a cooled reactor effluent stream; (b) passing
22 the cooled reactor effluent stream through an absorption column, thereby generating an
23 absorber bottoms stream that comprises water, acrylonitrile, and organic impurities; and
24 (c) passing the absorber bottoms stream through a single recovery/stripper column,
25 generating an acrylonitrile-rich overhead stream, a lean water side stream, and a
26 recovery/stripper bottoms stream that comprises organic impurities without an
27 enrichment column.

28 In an embodiment of the invention, the acrylonitrile-rich overhead stream is
29 passed through a decanter to separate water from acrylonitrile. In another specific

1 embodiment of the process, the lean water side stream is recycled for use in the
2 absorption column.

3 The present invention is more economical than prior art acrylonitrile processes.
4 Because it can achieve the desired level of product recovery without requiring both a
5 recovery distillation column, a stripper distillation column and/or an enrichment column,
6 both capital costs and operating costs are reduced.

7 In another embodiment, the invention relates to a system for the recovery of pure
8 acrylonitrile from an ammonoxidation reactor effluent stream comprising; (a) an
9 ammonoxidation reactor; (b) an absorption column; and (c) a single recovery and stripper
10 column, the system not including an enrichment column.

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13 **BRIEF DESCRIPTION OF THE DRAWINGS**

14 Figure 1 is a process flow diagram of a prior art acrylonitrile recovery process.

15 Figure 2 is a process flow diagram of an acrylonitrile recovery process of the
16 present invention.

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19 **DESCRIPTION OF ILLUSTRATIVE EMBODIMENTS**

20 Processes for producing olefinically unsaturated nitriles are well known in the art.
21 For example, an ammonoxidation process for producing acrylonitrile is disclosed in U.S.
22 patent 4,590,011, which is incorporated here by reference.

23 The production of acrylonitrile generally involves feeding propylene, ammonia, a
24 source of oxygen such as air, and an inert gas such as nitrogen to a fluidized bed reactor
25 zone where the reactants contact an ammonoxidation catalyst. The typical molar ratio of the
26 oxygen to olefin in the feed is from 0.5:1 to 4:1, preferably from 1:1 to 3:1. The molar
27 ratio of ammonia to olefin in the feed in the reaction is typically between 0.5:1 to 5:1.

28 Conditions for the ammonoxidation reaction to occur are well known in the prior art
29 as evidenced by U.S. patents 5,093,299, 4,863,891, 4,767,878, and 4,503,001, herein
30 incorporated by reference. The reaction is typically carried out at a temperature between
about 260° to 600°C, with 310° to 500°C being preferred, and with 350° to 480°C being

1 especially preferred. The contact time, although not critical, is generally in the range of
2 0.1 to 50 seconds, with a contact time of 1 to 15 seconds being preferred.

3 Preferably, the ammonoxidation reaction is performed in a fluid bed reactor although
4 other types of reactors can also be used. Fluid bed reactors, for the manufacture of
5 acrylonitrile are well known in the prior art. For example, the reactor design set forth in
6 U.S. patent 3,230,246, herein incorporated by reference, is suitable.

7 Catalysts for use in the reaction zone are well known in the art. Suitable catalysts
8 are disclosed in U.S. patents 3,642,930 and 5,093,299, herein incorporated by reference.

9 The reactor effluent will contain acrylonitrile, the desired product, plus organic
10 impurities such as acetonitrile, as well as some amount of excess reactants, all usually in
11 the gaseous state and at a temperature between about 450-480°C.

12 The reactor effluent is transported to a quench column (not shown) wherein the
13 hot effluent gases are cooled by contact with water spray. Typically, any excess ammonia
14 contained in the effluent is neutralized by contact with sulfuric acid in the quench to
15 remove the ammonia as ammonium sulfate. The cooled effluent gas containing the
16 desired product (acrylonitrile) is then passed into the bottom of an absorber column (not
17 shown) wherein the product is absorbed in water which enters the column from the top.
18 The non-absorbed gases pass from the absorber through a pipe located at the top of the
19 absorber. The aqueous absorber bottoms stream containing the desired product is then
20 processed for further purification.

21 Fig. 1 shows a prior art process for purification of the aqueous acrylonitrile-
22 containing stream from the absorber bottom. The aqueous stream 10 enters a first
23 distillation column or recovery column 12, which generates an overhead stream 14
24 containing water and acrylonitrile and a bottoms stream 16 that contains water and
25 various impurities, but relatively little acrylonitrile. The overhead stream 14 from the first
26 distillation column 12 passes through a condenser 18 and into a decanter 20 where water
27 and acrylonitrile are separated. The water stream 22 from the decanter can be recycled
28 for use elsewhere in the process. The product acrylonitrile stream 24 can be stored or
29 further purified if so desired.

1 The bottoms stream 16 from the first distillation column 12 is pumped to a second
2 distillation column or stripper column 30. A portion of the overhead 32 from this column
3 30, after passing through a condenser 34, is recycled 36 to the column 30, while another
4 portion 38 of that overhead is sent to waste treatment. The upper portion of the stripper
5 column 30 concentrates the volatile components (e.g., acetonitrile, etc.) of the mixture,
6 which is the enriching or rectifying section 31 of column 30, and stream 38 is made up of
7 concentrated acetonitrile. Heat is supplied to the recovery column 12 by means of stream
8 33, which is hot vapor made up of water and water miscible impurities. The bottoms
9 stream 40 from the second column 30 is also sent to waste treatment 42. A side stream
10 44 from the second column 30 is a lean water stream that can be recycled to the absorber
11 (not shown). A second side stream 46, containing water and a relatively small amount of
12 acrylonitrile, is recycled to the first distillation column 12, passing through a cooler 50.
13 Reboilers 26 and 48 supply energy for the distillation.

14 Although the recovery system of Fig. 1 will achieve the desired separation, it does
15 so at a relatively high cost, due to the dual distillation columns 12 and 30 with the
16 additional enrichment section 31, reboilers 26 and 48, the corresponding pumps 60, 62,
17 64, and 66, the associated piping, and the like, as well as the steam, cooling water, and
18 other inputs required to operate the recovery and purification process.

19 Fig. 2 shows an embodiment of an improved recovery system of the present
20 invention. The feed 10, again coming from the absorber bottoms, is fed to a single
21 distillation column 80. Whereas the first distillation column 12 and the second
22 distillation column 30 of Fig. 1 might for example have approximately 70 and 50 trays,
23 respectively, the single distillation column 80 of Fig. 2 might have for example
24 approximately 110 trays. Of course the present invention is not limited to columns
25 having any particular number of trays, nor is it limited to columns having trays at all.
26 Packed columns might be used instead.

27 A first side stream 82 contains primarily water and acetonitrile and is sent to
28 waste treatment. There is no need to enrich stream 82 and further separate acrylonitrile
29 from the acetonitrile as this stream 82 is substantially free of acrylonitrile (e.g., less than
30 1.0%, preferably less than 0.5%, and more preferably less than 0.3% by weight of the

1 crude acrylonitrile feed stream 10). Moreover, stream 82 is substantially free of hydrogen
2 cyanide (e.g., less than 1.0%, preferably less than 0.5%, and more preferably less than
3 0.3% by weight of the free hydrogen cyanide introduced in feed stream 10). Stream 82
4 includes substantially all of the acetonitrile (e.g., more than 99.0%, preferably more than
5 99.5%, and more preferably 99.7% by weight of the acetonitrile introduced via feed
6 stream 10). Accordingly, the present invention does not utilize an enrichment column. A
7 second side stream 84 is used as a lean water stream for recycle to the absorber. A third
8 side stream 86 passes through a cooler 88 and is recycled to the top 90 of the column 80.
9 A bottoms stream 92 is sent to waste treatment. A reboiler 94 supplies heat for the
10 distillation.

11 The overhead stream 96 from the combined recovery/stripper column 80 passes
12 through a condenser 98 and into a decanter 100, producing a product acrylonitrile stream
13 102 and a water stream 104 that can be recycled to the quench, the absorber, or the feed
14 stream 10.

15 Operating conditions for the distillation column 80 can vary depending on the
16 products to be recovered and the degree of recovery desired. For example, the column
17 could be operated at approximately atmospheric pressure at the inlet of the condenser 98.
18 The temperatures and pressures in other parts of the column would be dictated by the type
19 of column internals and the heat duty in the reboilers.

20 The process could be operated with the reboiler duty adjusted so that, for
21 example, 99.9% by weight of the acrylonitrile and 99.4% of the free hydrogen cyanide in
22 the absorber bottoms stream 10 can be recovered in the overhead stream 96. In addition,
23 by adjusting the flow rate and temperature of the stream 86 which is recycled to the top
24 90 of the column, the overhead stream 96 can contain as little as 0.3% of the acetonitrile
25 from stream 10. In other words, 99.7% of the acetonitrile in the absorber bottoms stream
26 10 can be removed and sent to waste treatment via stream 82.

27 The manner of operation described in the preceding paragraph is suitable in
28 situations where hydrogen cyanide is a valuable byproduct and therefore is intended to be
29 recovered to the extent practical. In situations where there is no need to recover that
30 compound, the process could instead be operated with reduced reboiler duty.

1 In another embodiment, the invention relates to a system for the recovery of pure
2 acrylonitrile from an ammonoxidation reactor effluent stream comprising: (a) an
3 ammonoxidation reactor; (b) an absorption column; and (c) a single recovery and stripper
4 column, the system not including an enrichment column.

5 The system recovers at least about 99.0% by weight, preferably about 99.5% by
6 weight, and more preferably about 99.7% by weight of acrylonitrile from the crude
7 acrylonitrile fed into the recovery and stripper column, without the use of an enrichment
8 column.

9 The amount of process equipment required for the recovery process of Fig. 2 is
10 significantly less than for the process of Fig. 1. The desired recovery of acrylonitrile is
11 still possible despite the reductions in equipment requirements and the resulting reduction
12 in operating cost. In particular, the elimination of the condenser and reflux required by a
13 second distillation column and/or an enrichment column lowers overall steam usage. In
14 addition, since a condenser is eliminated, cooling water usage is reduced.

15

16 The preceding description of specific embodiments of the present invention is not
17 intended to be a complete list of every possible embodiment of the invention. Persons
18 skilled in this field will recognize that modifications can be made to the specific
19 embodiments described here that would be within the scope of the present invention.

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